**Development** and commissioning of an innovative biorefinery for the conversion of contaminated biomass into high-quality energy carriers



Fraunhofer Institute for Environmental, Safety and Energy Technology UMSICHT

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5 – 8 June | Conference & Exhibition 9 June | Technical Tours





# Agenda











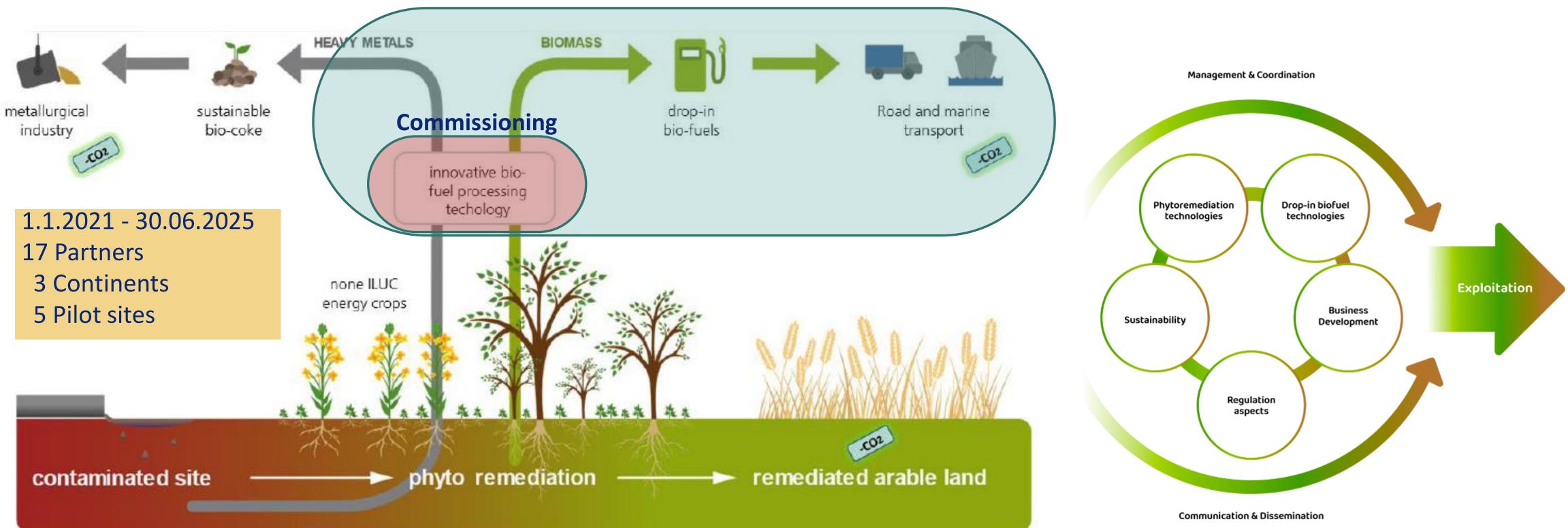








# Phy2Climate - Combining phytoremediation with biofuel generation













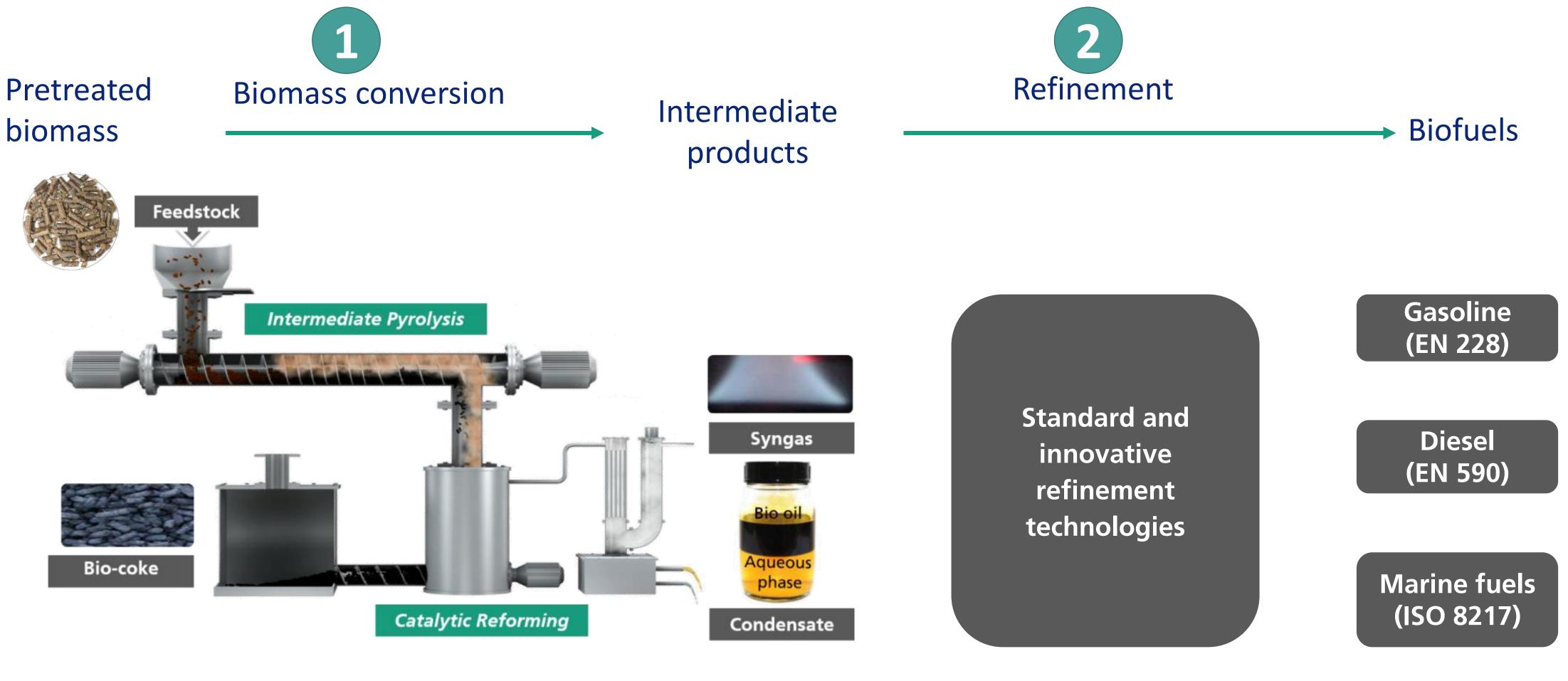
#### **Focus of Fraunhofer UMSICHT**







# **Definition of the Phy2Climate biorefinery**















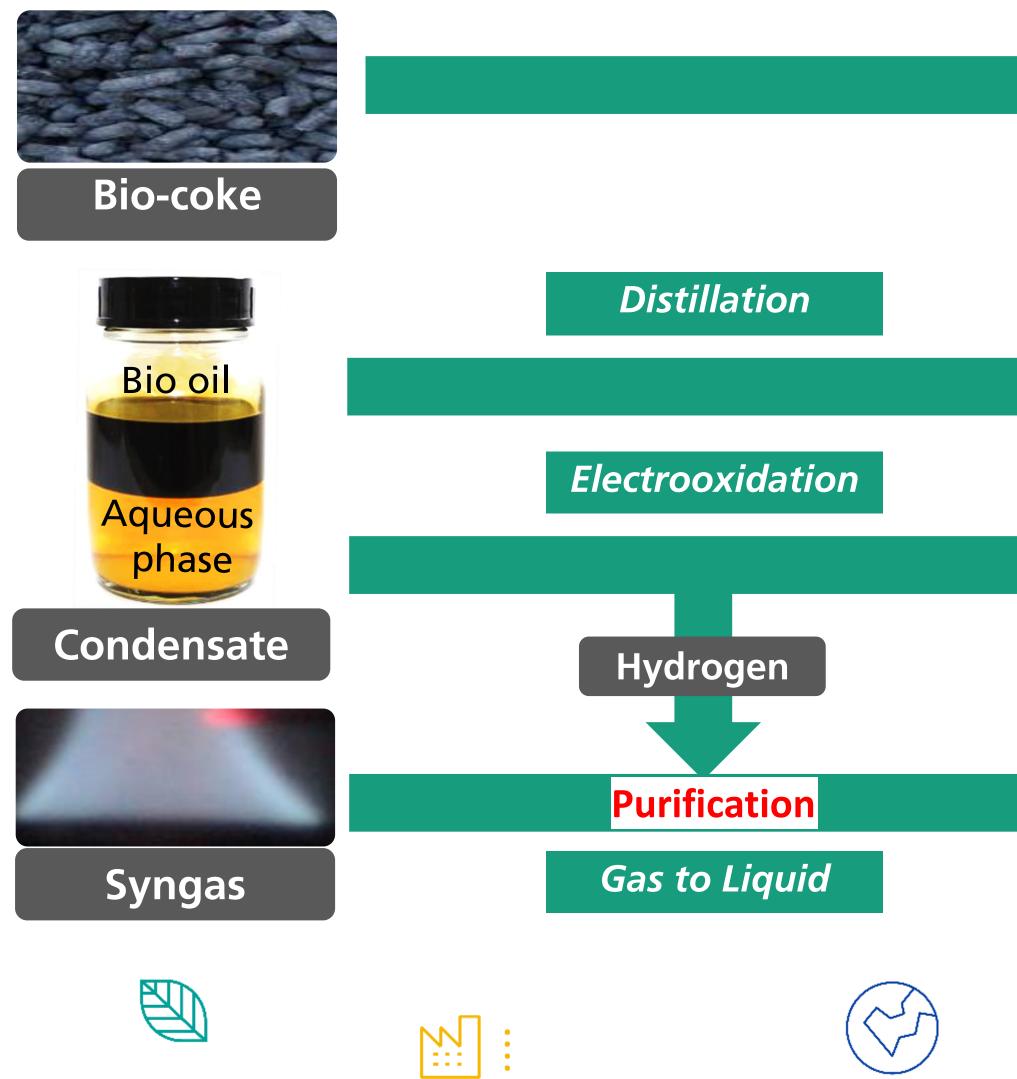








# **TCR-product refinement within Phy2Climate**

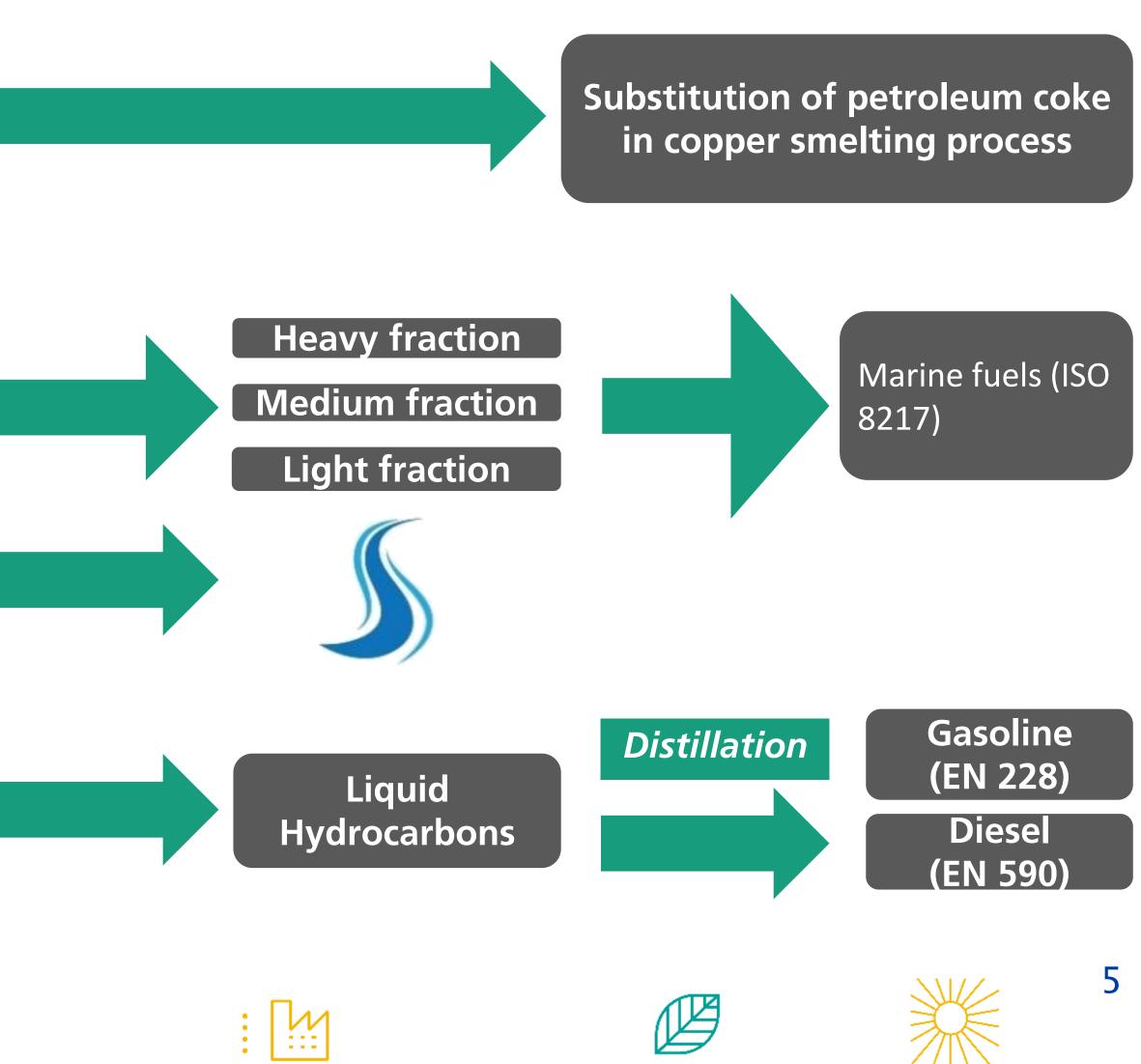






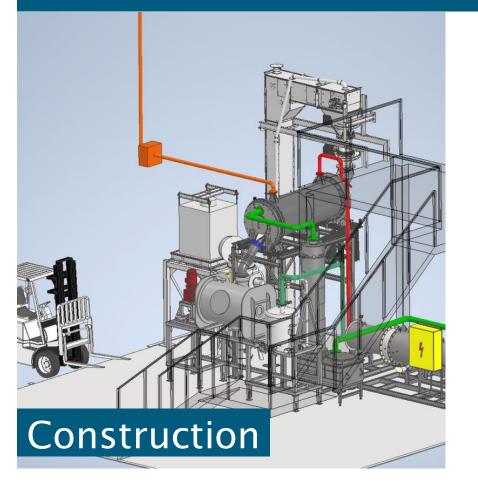






# Challenges in commissioning the biorefinery

- Managing the interfaces of the single biorefinery parts
- Design and commissioning of new biorefinery parts (e.g. gas purification unit)
- Assembly of the biorefinery because of bottlenecks in the supply chain















From innovation to application





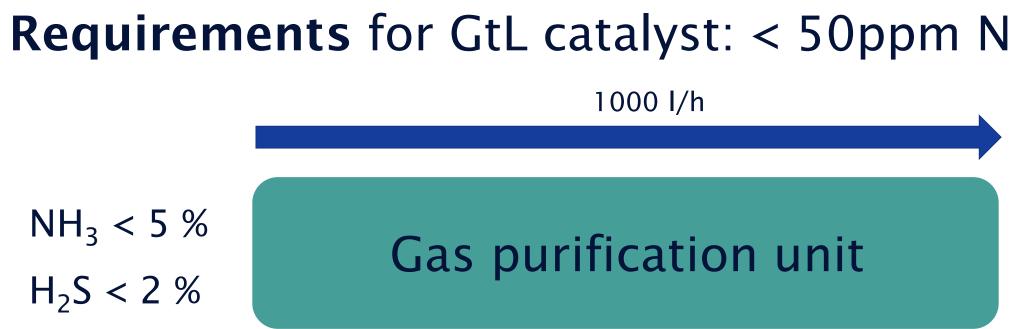




# Purification of TCR gas - critical gas components

### Initial situation

- TCR<sup>®</sup> process at 1000 l/h gas flow rate
- Ammonia (NH<sub>3</sub>) up to 5vol.-%
- Hydrogen sulfide (H<sub>2</sub>S) between 0.5% and
- HCN, COS, HCL, Br, F, alkalis













TCR gas composition with sewage sludge as feed, PR: 600°C

	Gas component	as component Fraction in vol%		
	H <sub>2</sub>	34.2		
d 2%	СО	11.6		
	CO <sub>2</sub>	24.2		
NH <sub>3</sub> and H <sub>2</sub> S	CH4	0.04		
	$C_xH_y$	1.06		
	NH3	< 5		
NH <sub>3</sub> < 50 ppm	H <sub>2</sub> S	0,5 - 2		
H <sub>2</sub> S < 50 ppm				









# TCR gas cleaning - strategy & technical design

#### **Gas scrubbers**

- Acidic (initial cleaning of NH<sub>3</sub>)
- Basic (initial cleaning of H<sub>2</sub>S)
- $\rightarrow$  operated in series, filled with packing

#### **Fixed bed reactors**

- Final cleaning of H<sub>2</sub>S
- $\rightarrow$  iron oxide pellets as reaction agent

operated alternately

### **Cooling trap**

- 2-step process for removal of H<sub>2</sub>O and NH<sub>3</sub>
  Fixed bed reactors
- For removal of HCN, COS, HCL, Br, F and alkalis

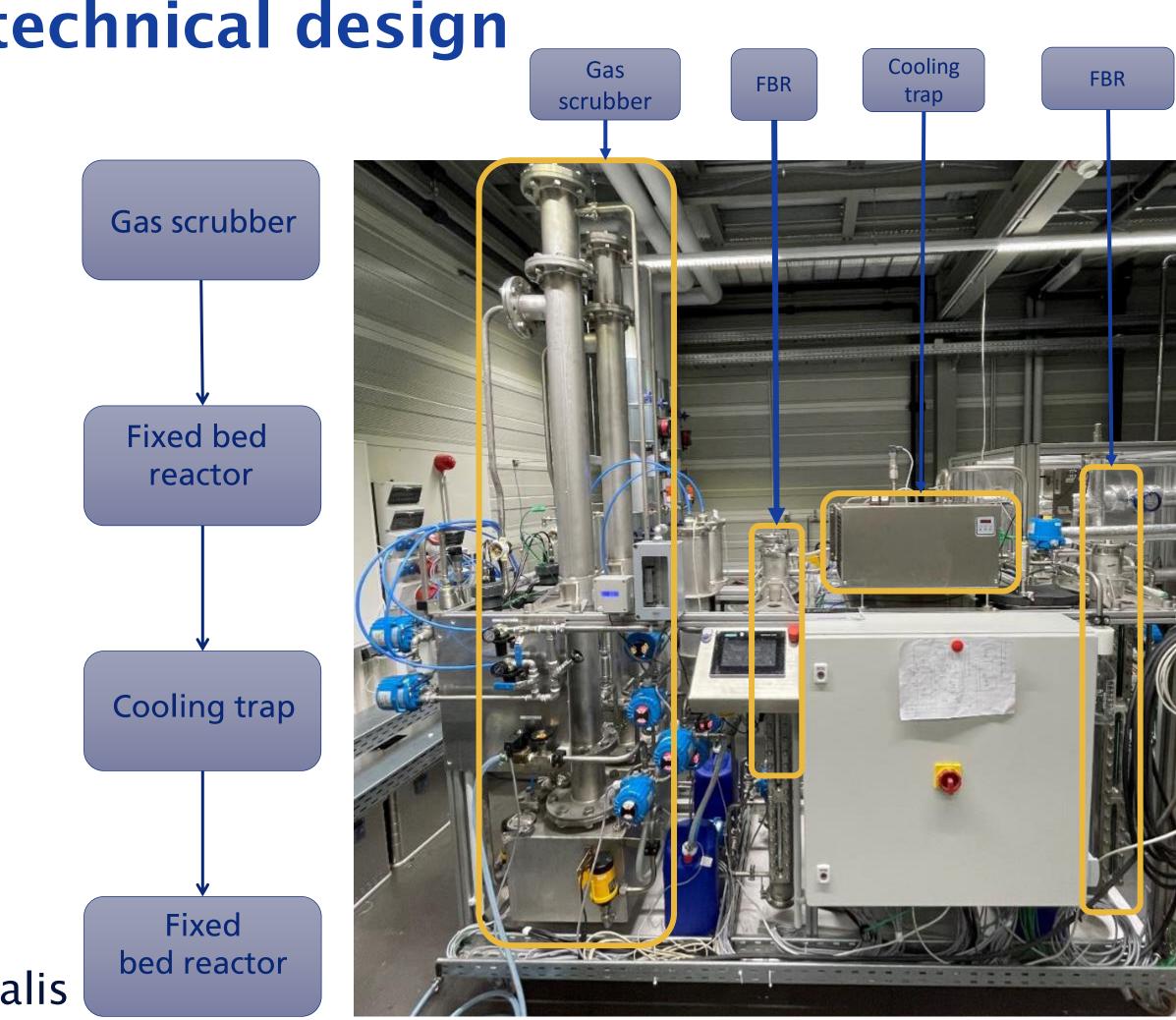










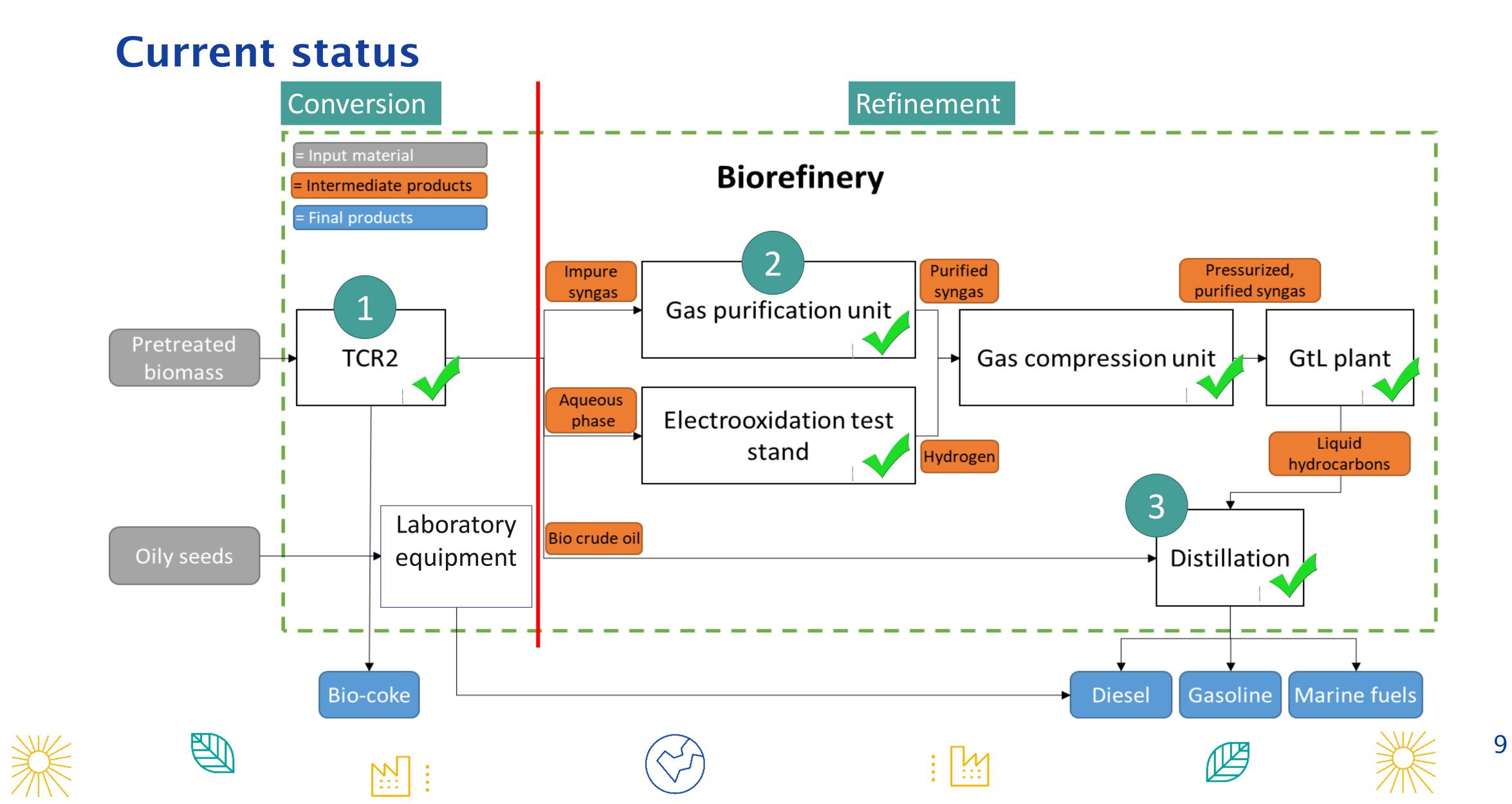














# **First results - Overview of conversion trials**

### Feedstock origins and TCR trials carried-out

Feedstock origin	Soil contamination	Used plant species for phytoremediation	Reactor temp. (°C)	Postreformer temp. (°C)
Lithuania Petroleum hydrocarbons	Petroleum hydrocarbons	Tall fescue, Perennial	450	750
	ryegrass, Alfalfa, Festuca perennis, Bird's-foot trefoil	450	650	
		450	550	
Serbia (Cr; Cu; Zn; Cd; Pb; Ni / Petroleum hydrocarbons, organochlorine pesticides)	Brassica napus	450	750	
		450	650	
		450	550	

Analysis done













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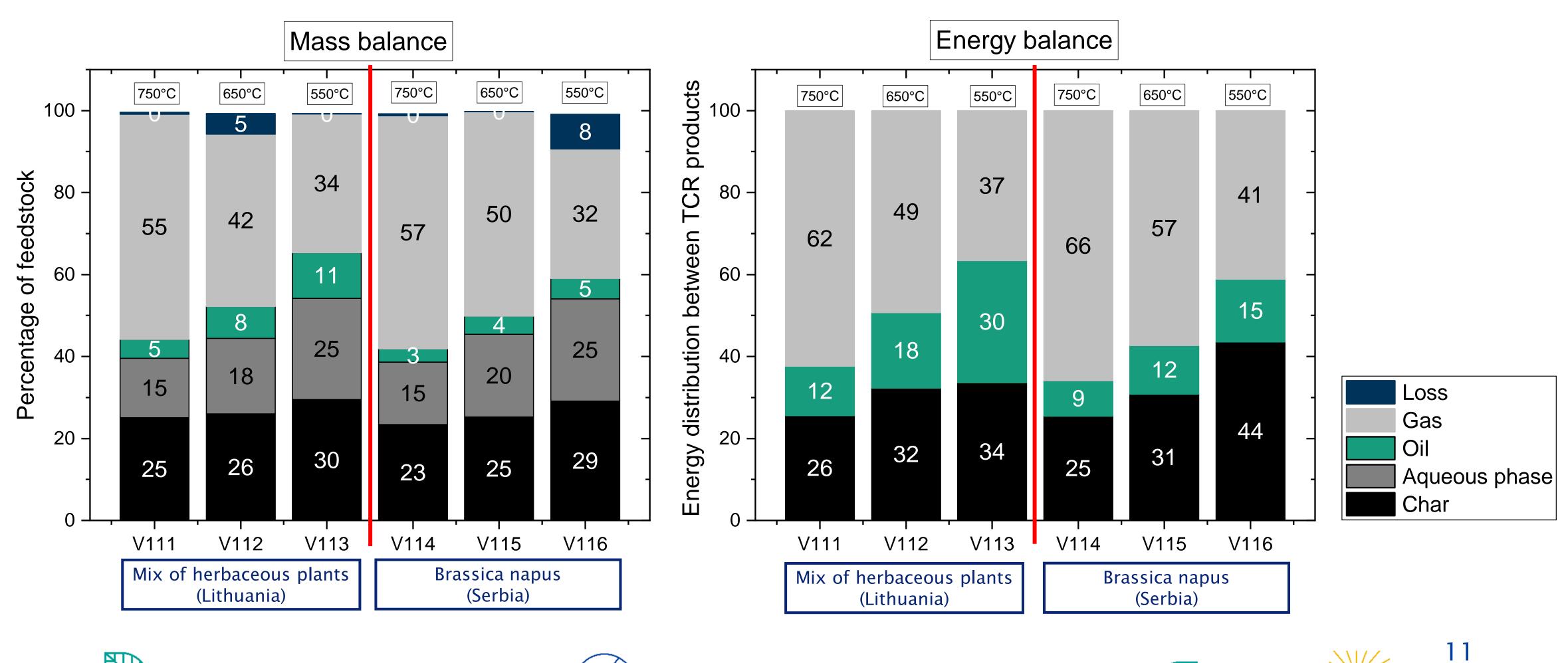




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# First conversion results - Mass- and energy balances











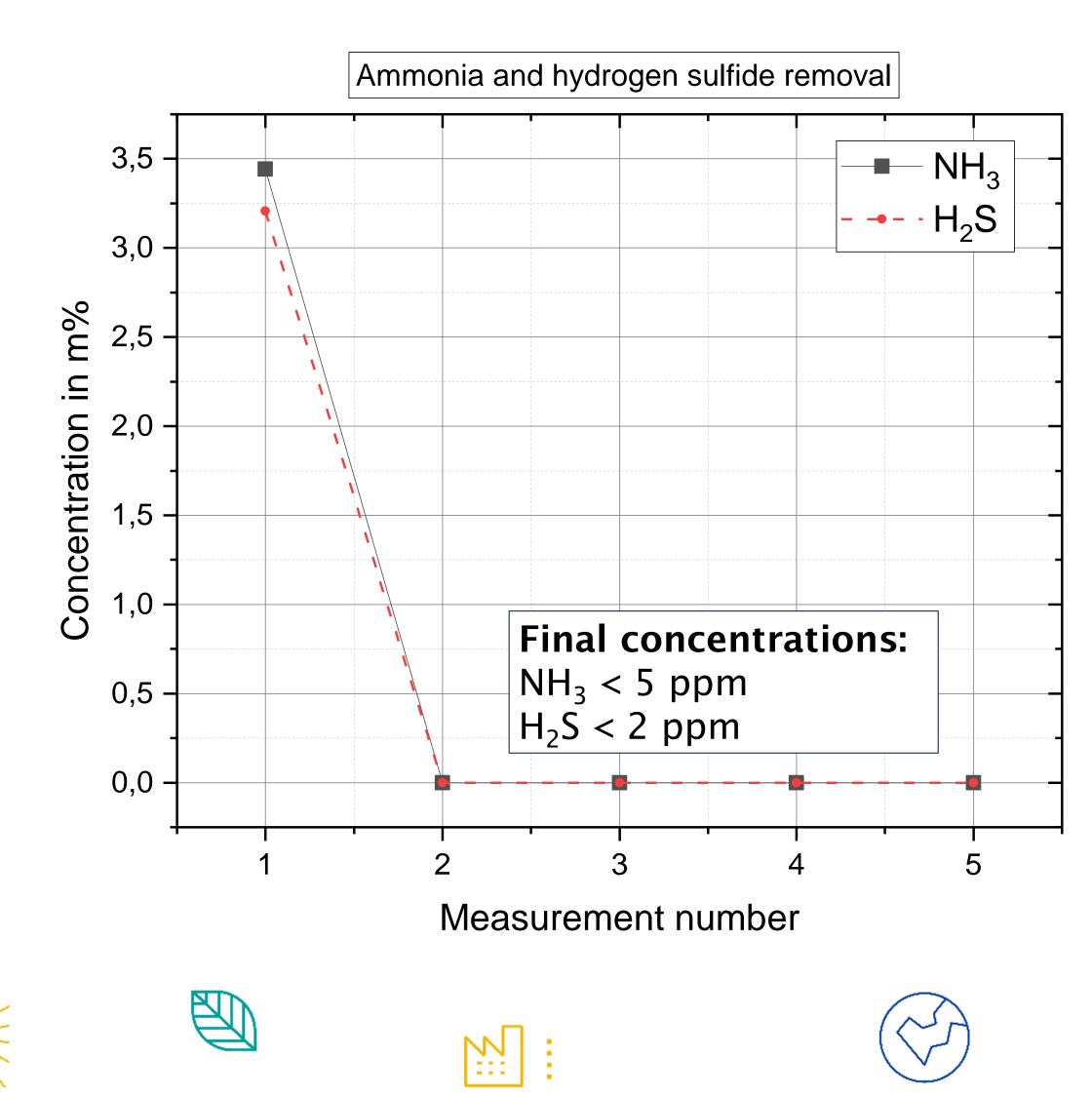




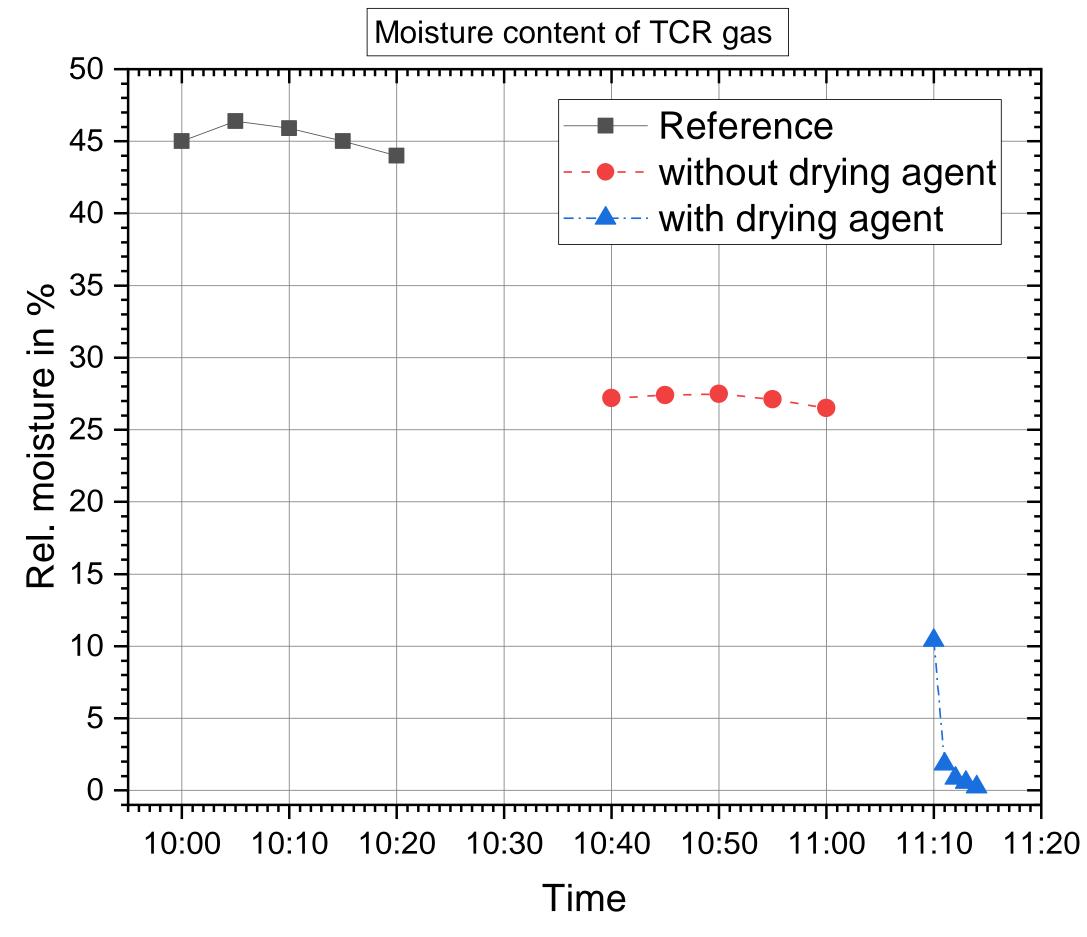




# First refinement results - TCR-gas purification















# First refinement results - TCR-oil distillation

### Boiling cuts: 150°C and 250°C



Next steps: Analysis of distillation products according to ISO 8217:2017 Petroleum products - Fuels (class F) - Specifications of marine fuels











#### Oil phase < 150°C Oil phase < 250°C Oil phase > 250°C







# **Summary and Outlook**

## Things successfully achieved so far:

- Designing, assembling and commissioning of a biorefinery
- First conversion trials
- First product refinement

### Next steps:

- Further conversion trials
- Development of a mass and energy concept of the overall biorefinery









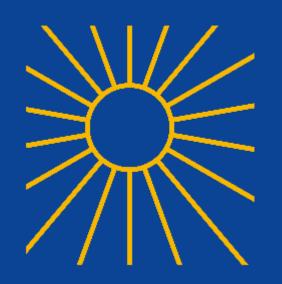


# Ongoing refinement of intermediates & evaluation according to the project goals











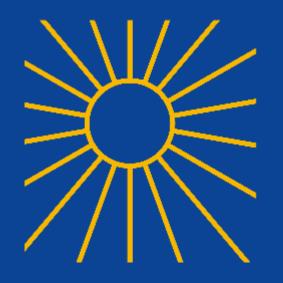






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# Thank you





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